

# **ROBUST DESIGN VIA OPERABILITY**

**57<sup>th</sup> CScE Conference**

**Session on Process Design and Analysis**

**October 29, 2007, Edmonton, Alberta**

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**And McMaster Advanced Control Consortium**

[www.macc.mcmaster.ca](http://www.macc.mcmaster.ca)



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UNIVERSITY**

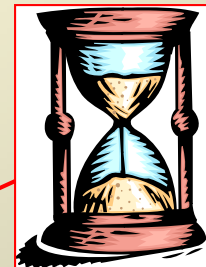


**1280 Main Street West, Hamilton, ON, Canada L8S 4L7**

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# GOALS OF THE PRESENTATION

- Provide a (not the) definition of operability
  - A taxonomy of issues
- Demonstrate that operability is not a collection of “tricks”
  - Improves teaching of **fundamentals**
  - Motivates students to **learn/apply**
- **Whet your appetite**, refer to WEB site for expanded coverage – **with workshops**
- Suggest that instructors **share teaching materials** to improve our understanding and to reduce teaching load

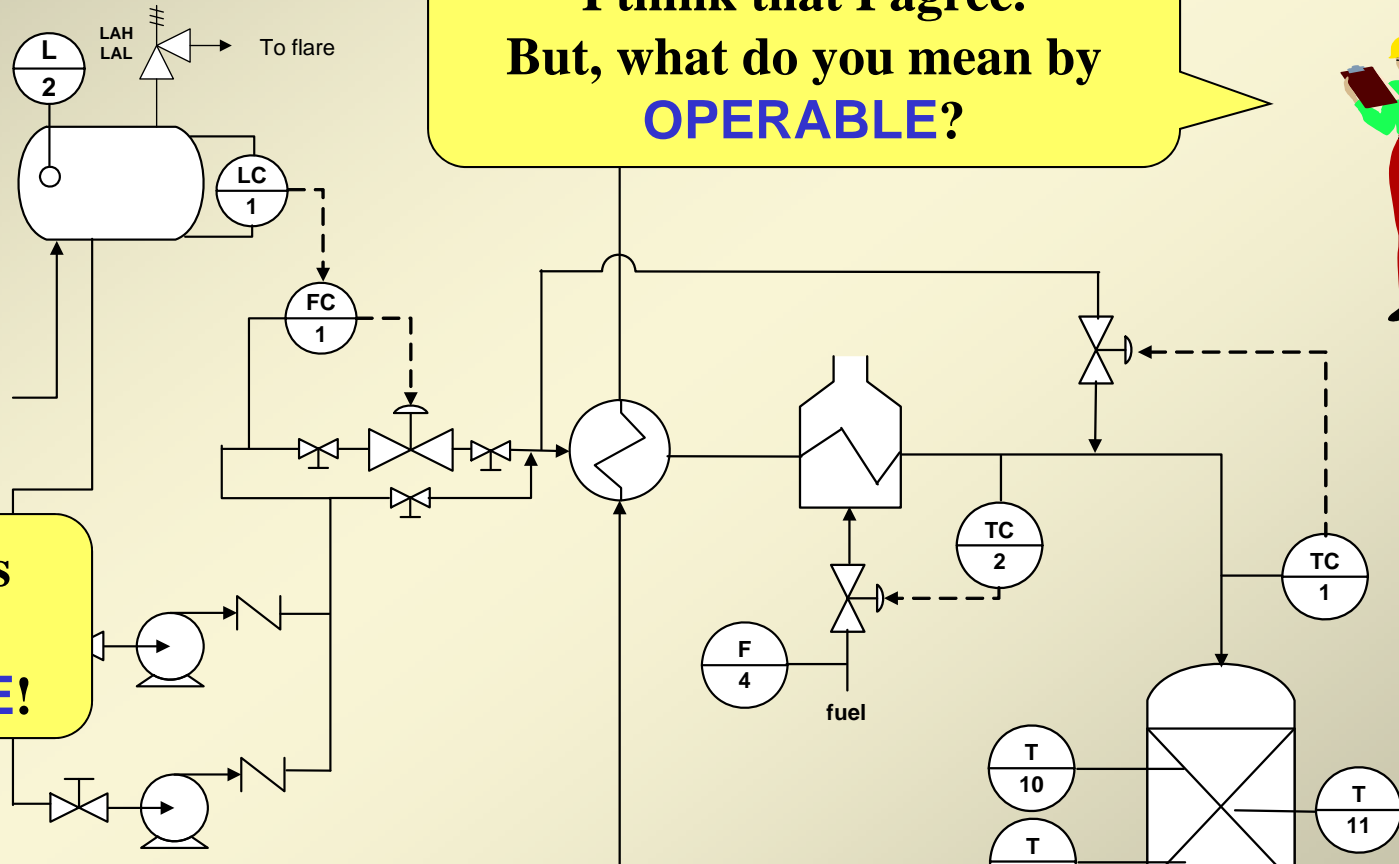


**Too  
little  
time!**

# WE DO NOT HAVE A CONSISTENT UNDERSTANDING OF THE ISSUES INVOLVED IN OPERABILITY

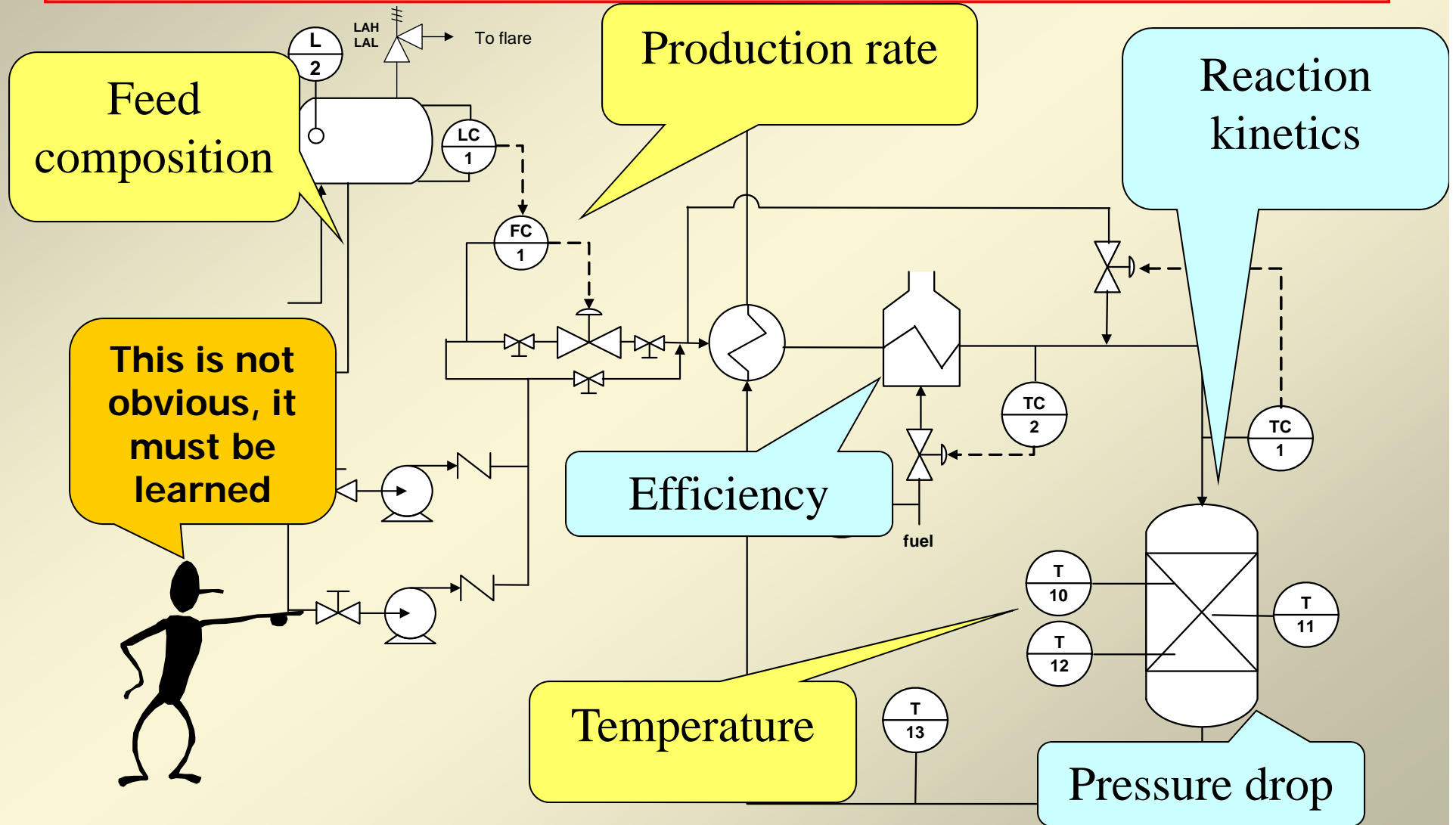
I think that I agree.  
But, what do you mean by  
**OPERABLE?**

The process  
must be  
**OPERABLE!**



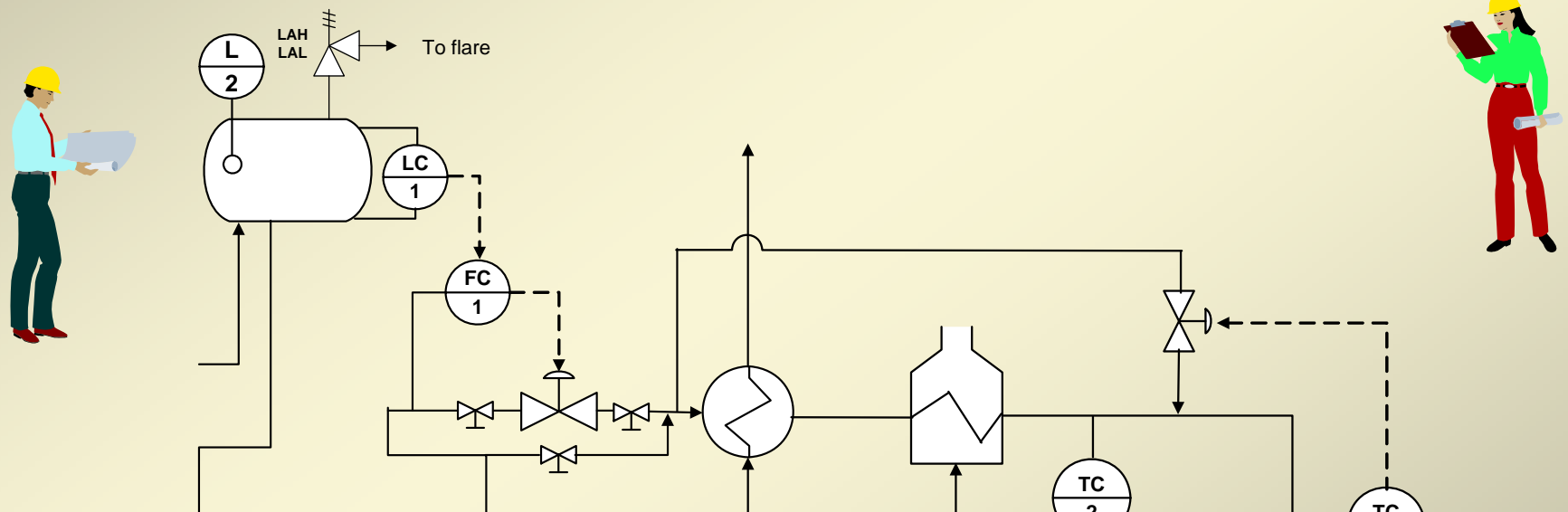
We have recently encountered a communication difficulty, so  
**Process Operability = Robust Design**

# OPERABILITY BECOMES ESSENTIAL WHEN WE CONSIDER REALISTIC VARIABILITY AND UNCERTAINTY



# OPERABILITY CAN NOT BE “ADDED-ON” AT THE END OF THE DESIGN

We must introduce appropriate equipment to ensure that a process is operable



**“The principle sins of flowsheets used for economic evaluation are sins of omission ... frequently omitted items include storage tanks, surge tanks, duplicated equipment (for reliability), startup equipment, emergency safety equipment, ..” (Valle-Riestra, 1983).**

## CRITERIA FOR SELECTING OPERABILITY TOPICS

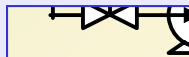
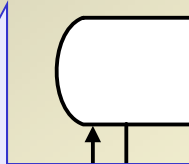
- **Generic** issues that apply to wide range of systems
- Reinforce **fundamental** principles
- Introduce common issues and solutions in engineering practice
  - Not comprehensive for any particular process
  - Demonstrates principles, students can expand to other issues and technical solutions
  - Leading to **respect for making a real physical system function**
- Prepares for performing a **major project**

**Key Operability issues**

1. Operating window
2. Flexibility/controllability
3. Reliability
4. Safety & equipment protection
5. Operation during transitions
6. Dynamic Performance
7. Efficiency
8. Monitoring & diagnosis

**IS THIS**

Feed tank



**Key Operability Topics**

1. Operating window
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**Key Operability  
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1. Operating window
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diagnosis

## Key Challenge

**How do we enable students to solve complex problems with multiple objectives?**

- **Provide superstructure for knowledge**
- **Tie to professional skills: problem solving, group skills, report writing, oral presentation, etc.**
- **Link to basics**
- **Show compelling, practical examples (within the students grasp)**
- **Encourage (require) students to **investigate, discover and evaluate issues in real processes****



**Key Operability issues**

1. Operating window

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# OPERATING WINDOW

What determines the window?

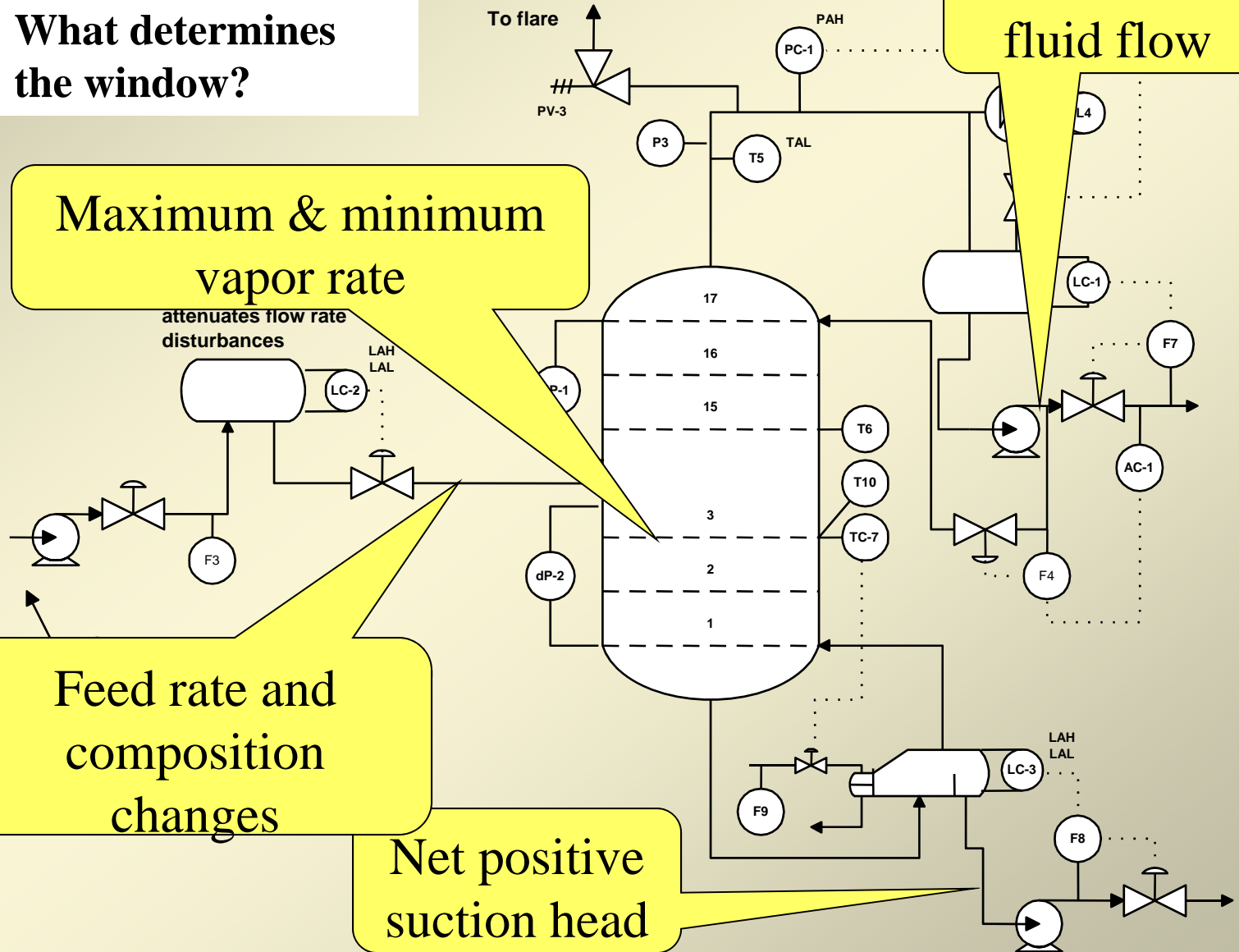
Maximum & minimum vapor rate

attenuates flow rate disturbances

Feed rate and composition changes

Net positive suction head

Maximum fluid flow





Key Operability issues

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controllability

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5. Operation during transitions

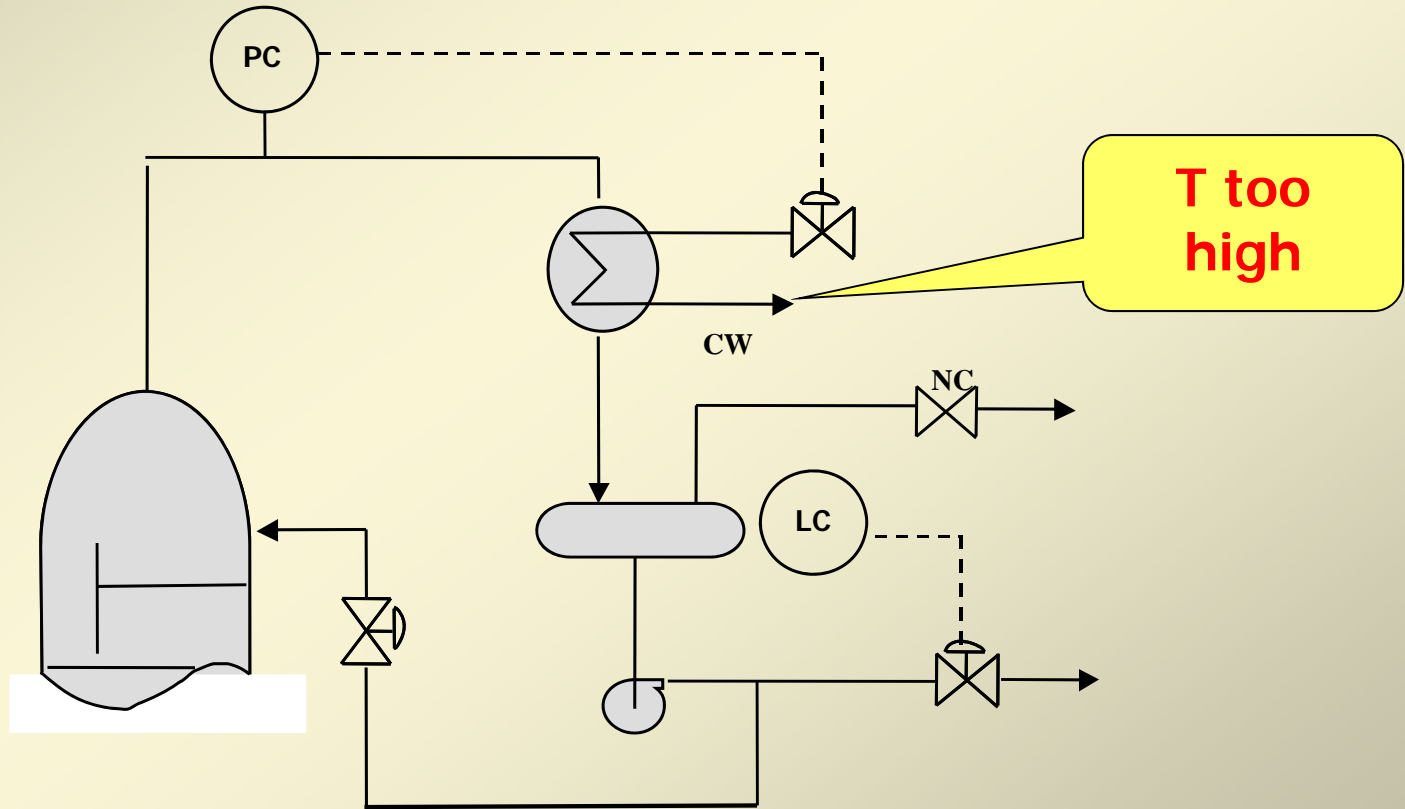
6. Dynamic Performance

7. Efficiency

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# FLEXIBILITY AND CONTROLLABILITY

$$Q = UA(\Delta T) \text{ Which to influence?}$$



**Not recommended!**



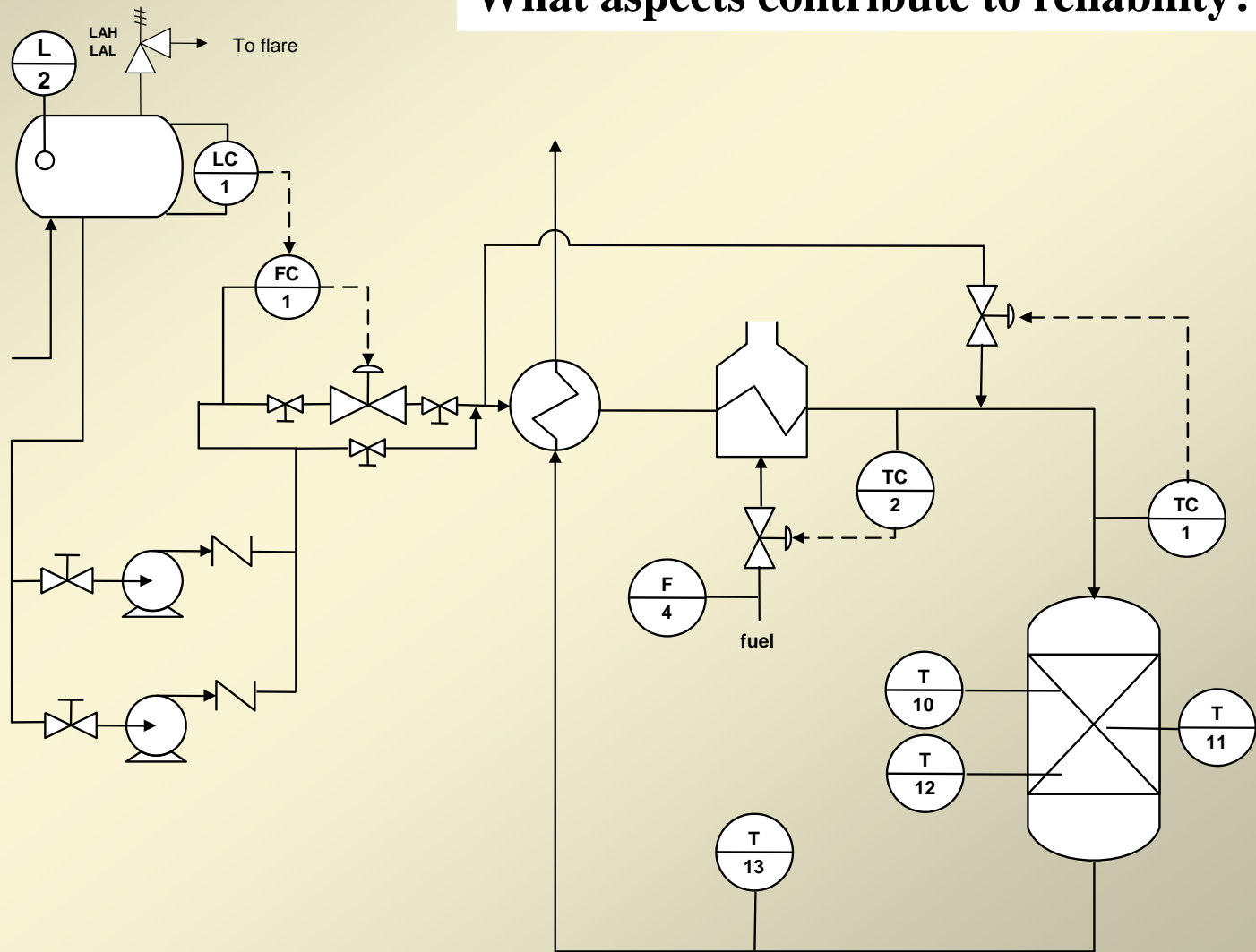


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# RELIABILITY

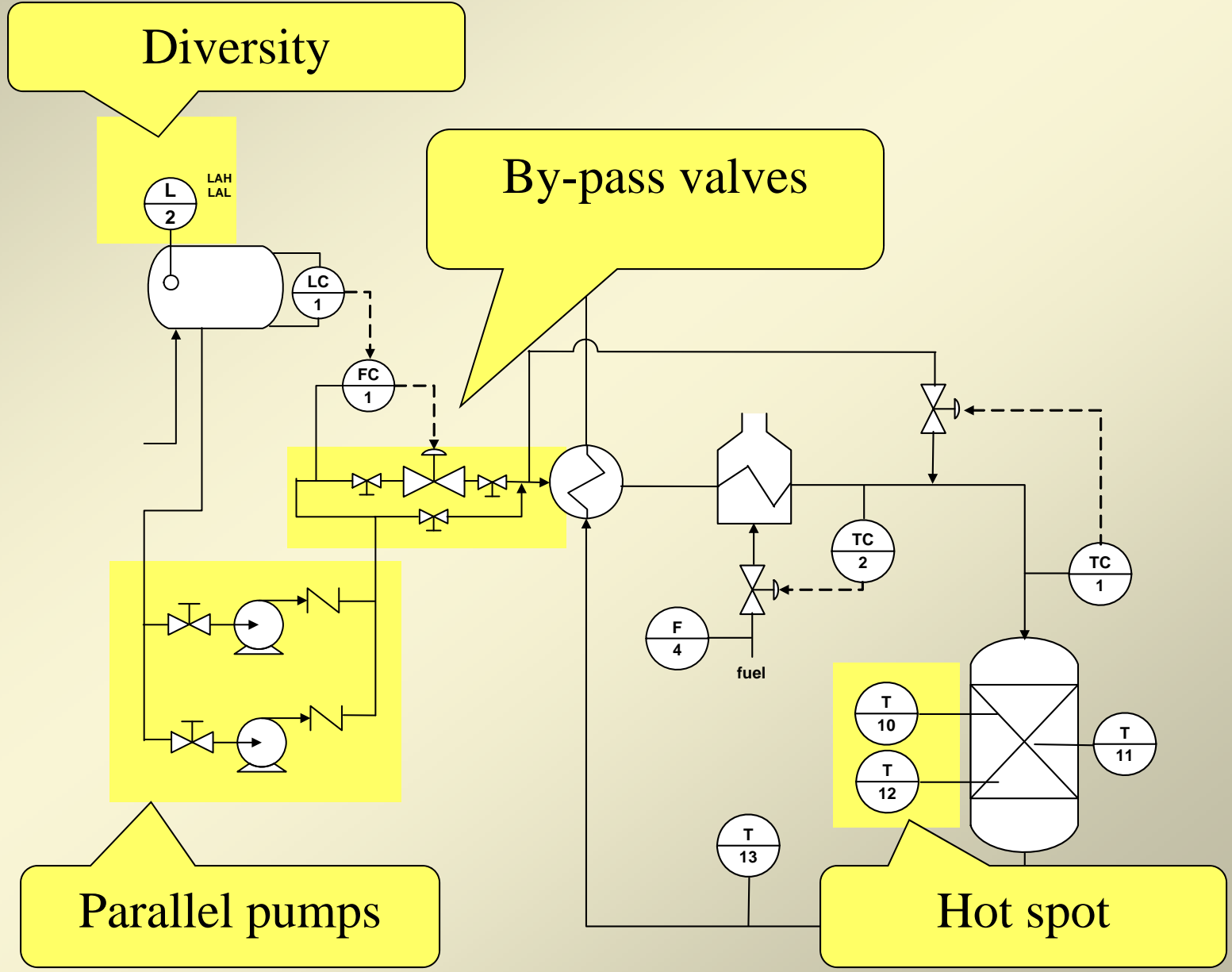
What aspects contribute to reliability?



**Key Operability issues**

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# RELIABILITY

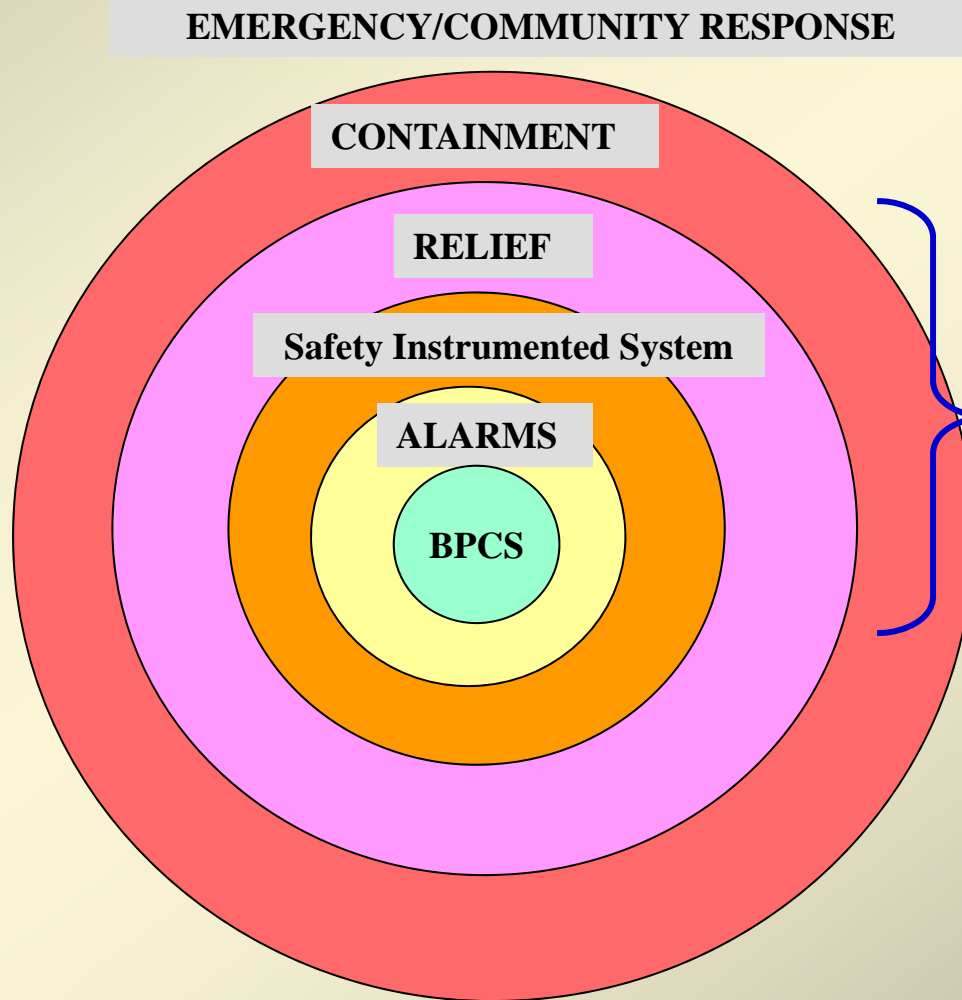


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# SAFETY & EQUIP. PROTECTION

## Layers of Safety Protection



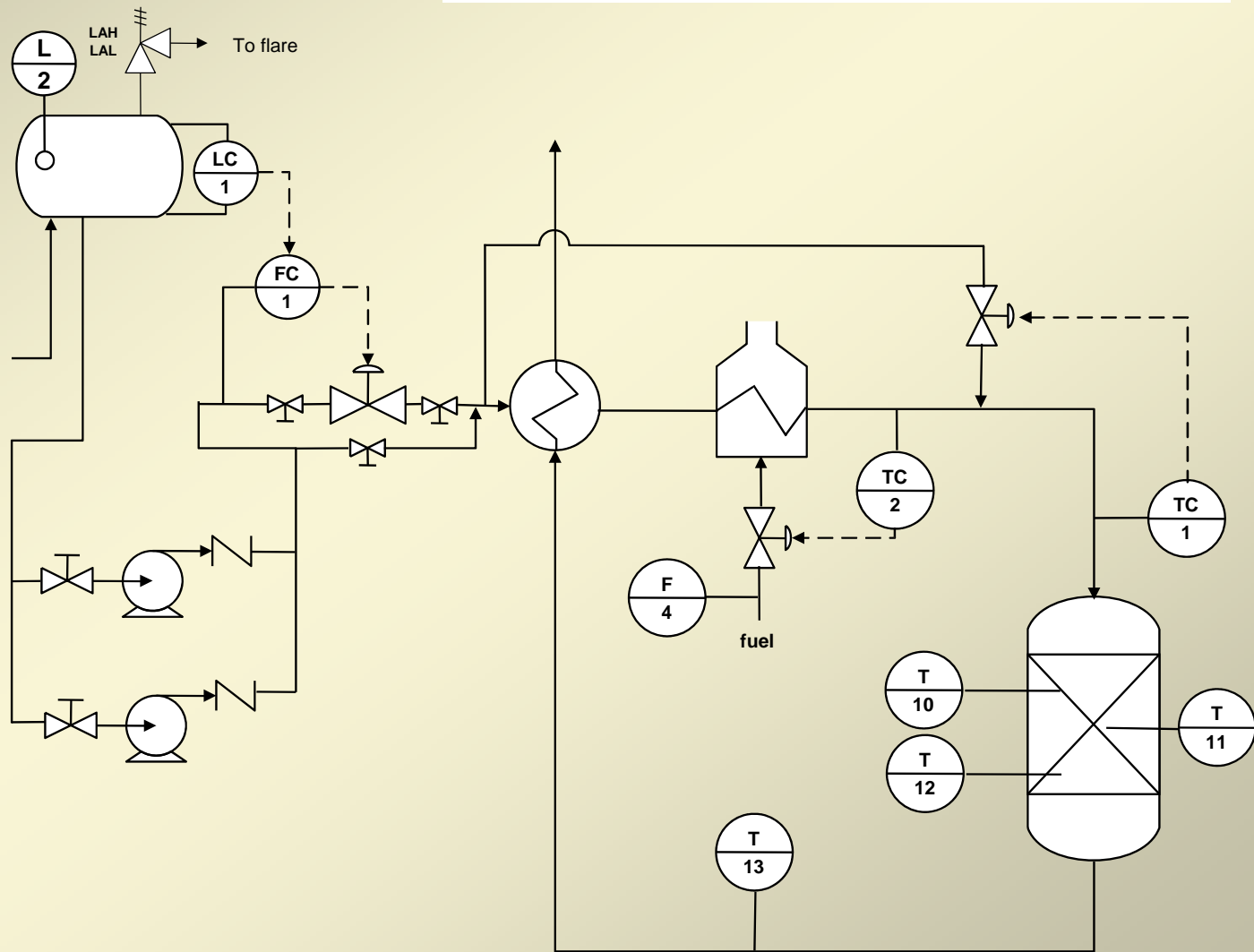
- Concentrate on the first four layers
- Stay close to the process

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# SAFETY & EQUIP. PROTECTION

What aspects contribute to safety?

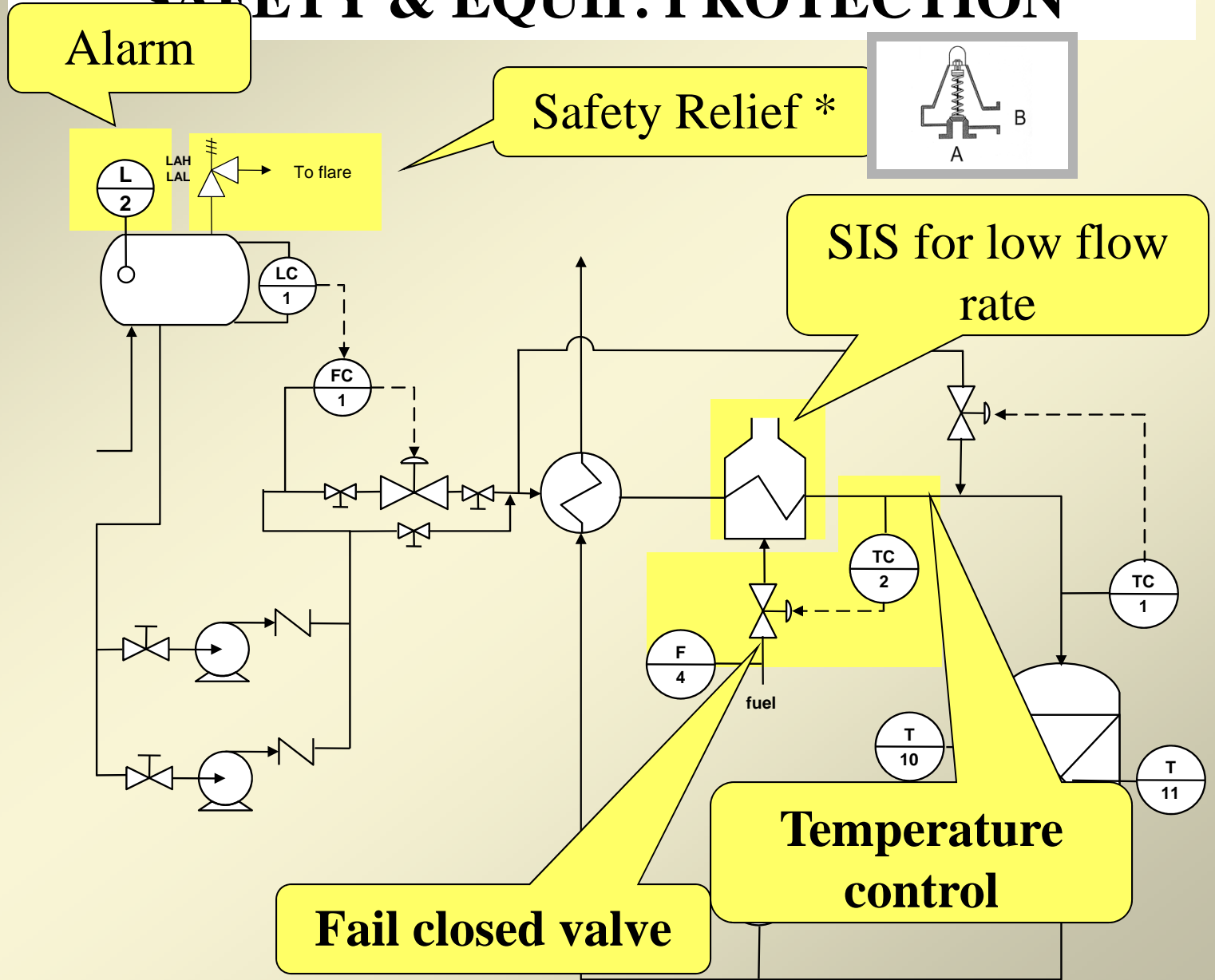




**Key Operability issues**

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# SAFETY & EQUIP. PROTECTION



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# SAFETY & EQUIP. PROTECTION



**HAZOP method provides a structured manner for safety analysis (using qualitative analysis)**

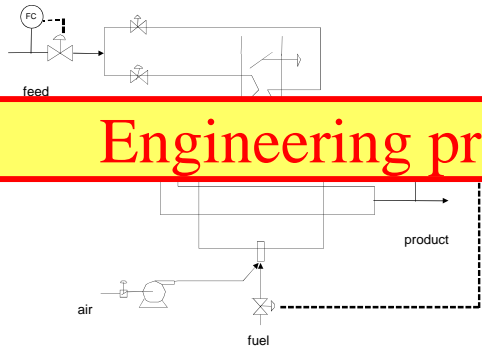
Unit: Fired heater Note the specific location

Node: air pipe after compressor and valve      Parameter: Pressure

Guide Word	Deviation	Cause	Consequence	Action
lower	Low pressure in the fuel pipe node	Stoppage of power to motor or turbine turning the compressor	Uncombusted fuel in the fire box – danger of explosion  Uncombusted fuel – wasted fuel	SIS based on the rotation of motor shaft *
		Break of coupling between motor and compressor	“	SIS based on rotation of compressor shaft*
		Failure of compressor, e.g., bending of blades	“ (plus danger from flying metal)	
		Failure of air valve due to failure	“	Fail open valve
		Any of the above	“	SIS that measures the flow of air after the pipe and activates the shutdown if the flow is too low
		Closure of air valve due to poor decision by operator	“	Air flow controller with ratio to fuel flow

**Principles**

**Engineering practice**



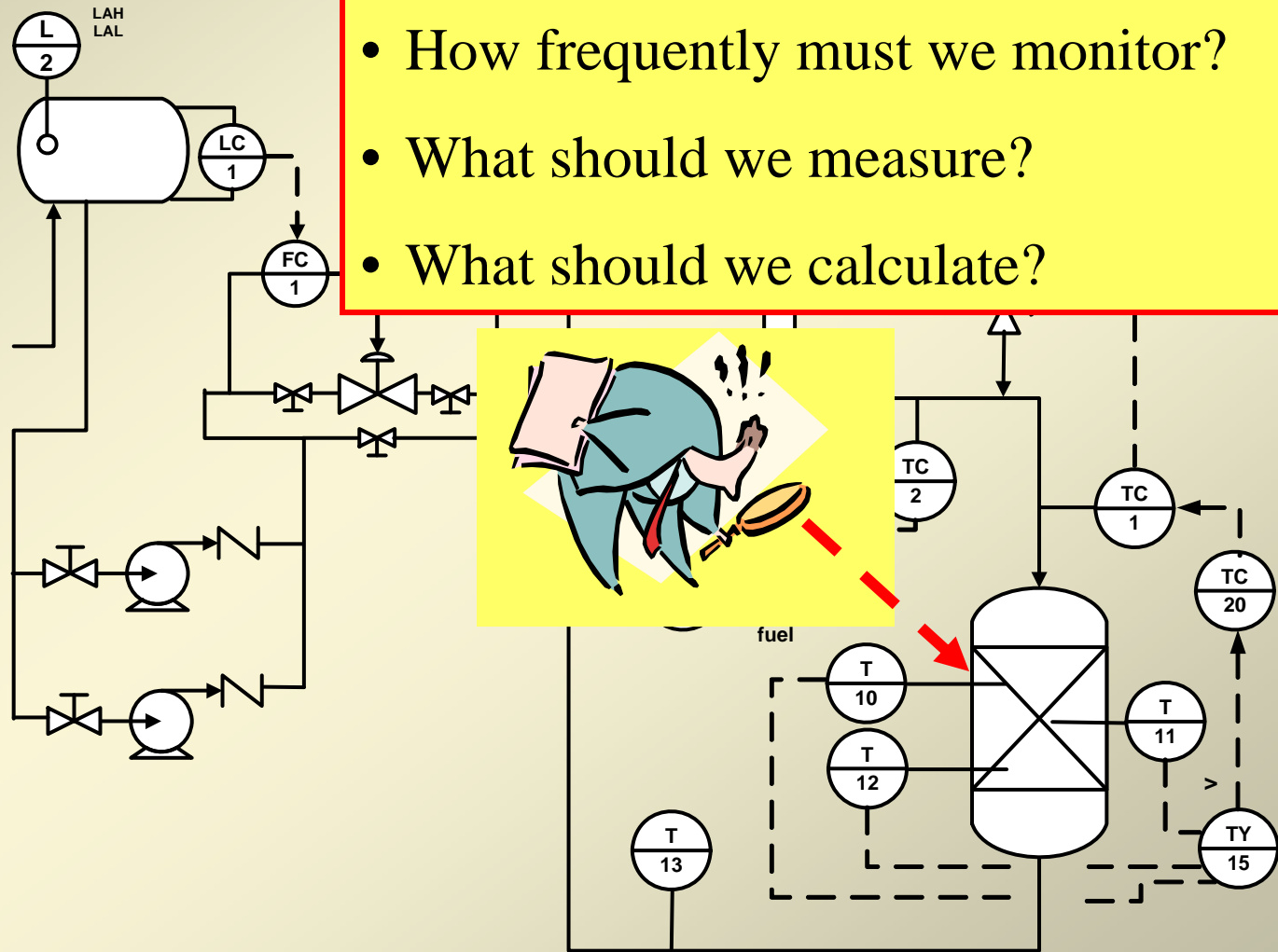
**Key Operability issues**

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# MONITORING & DIAGNOSIS

- What is important?
- How frequently must we monitor?
- What should we measure?
- What should we calculate?

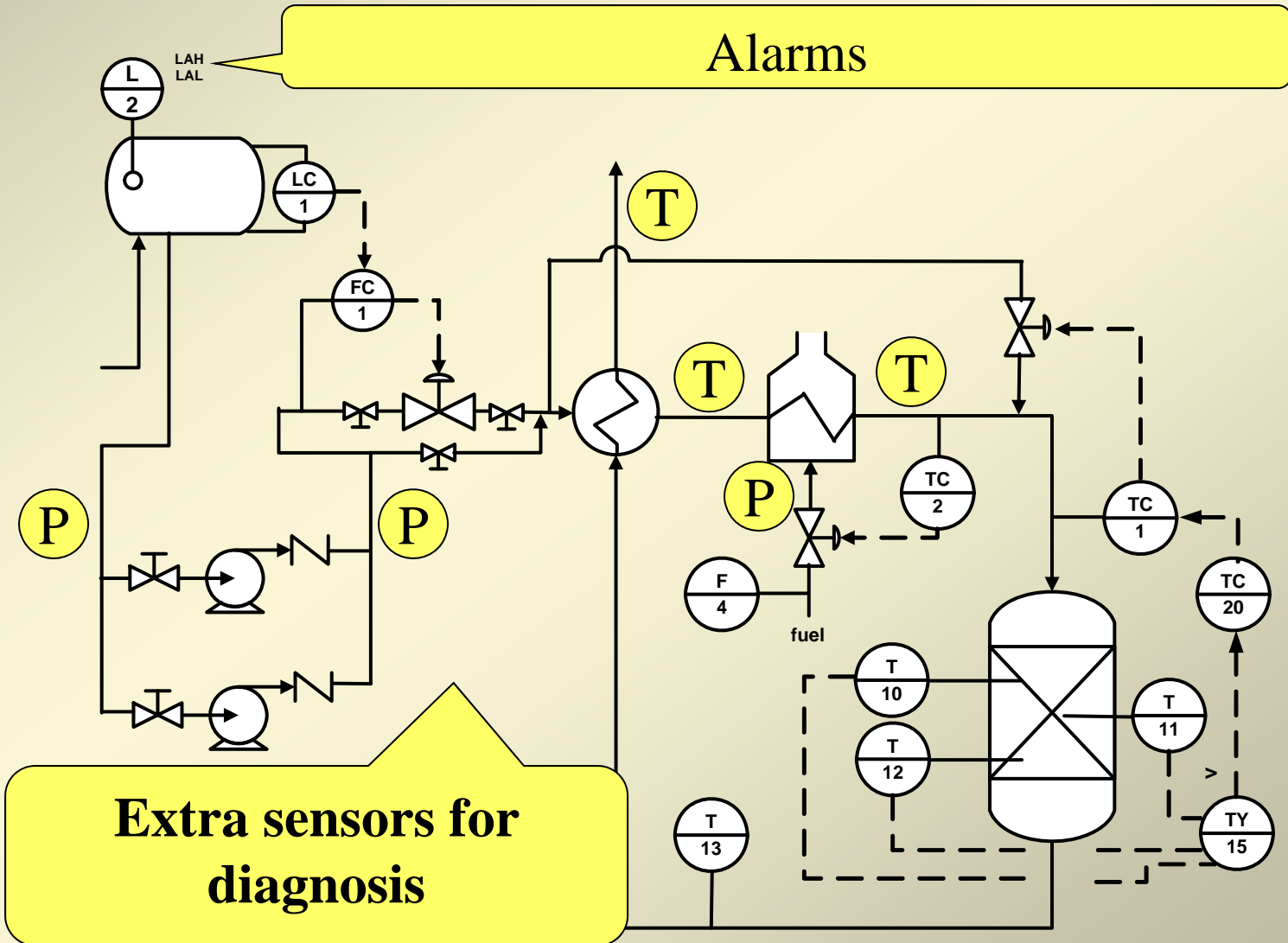


**Key Operability issues**

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# MONITORING & DIAGNOSIS

**Rapid decisions** – made by operating personnel



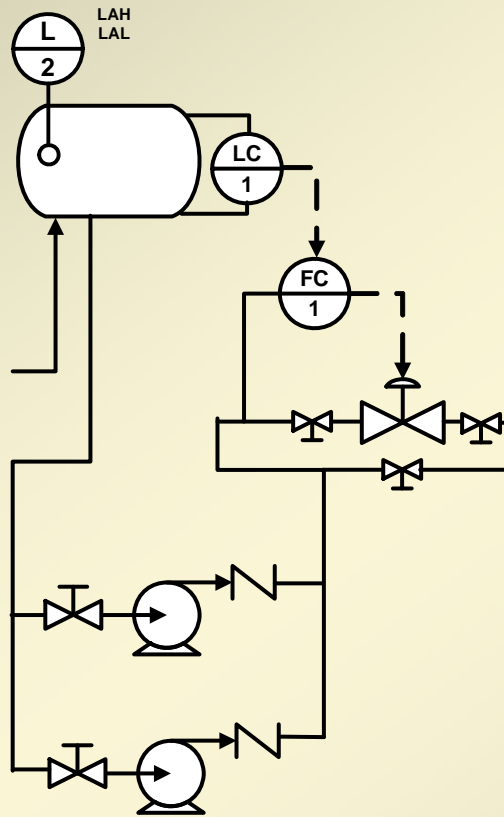
Key Operability issues

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# MONITORING & DIAGNOSIS

**Longer-term** decisions – made by engineers



## MONITOR

- Heater efficiency
- Reactor conversion and selectivity
- Material balance
- Exchanger fouling
- Pressure drops through system
- Time each pump in service

**Sensors + Calculations!**

**Key Operability issues**

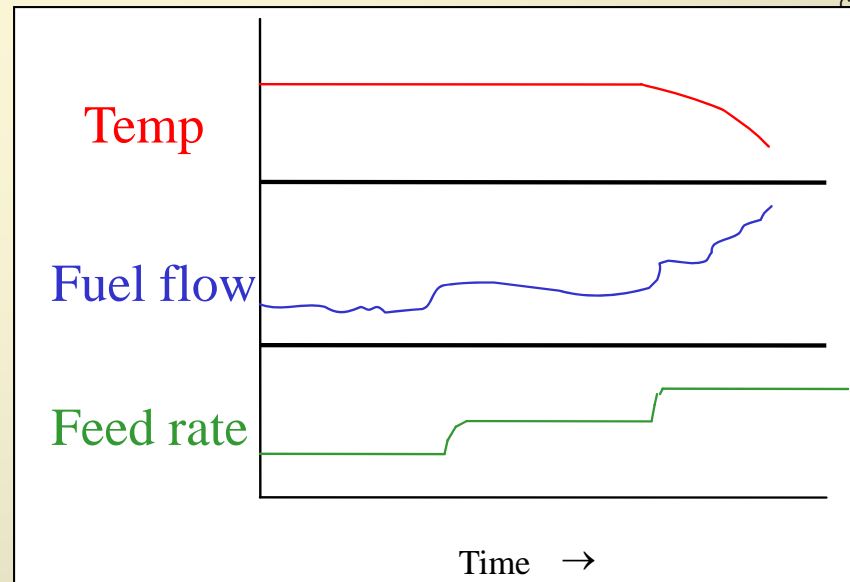
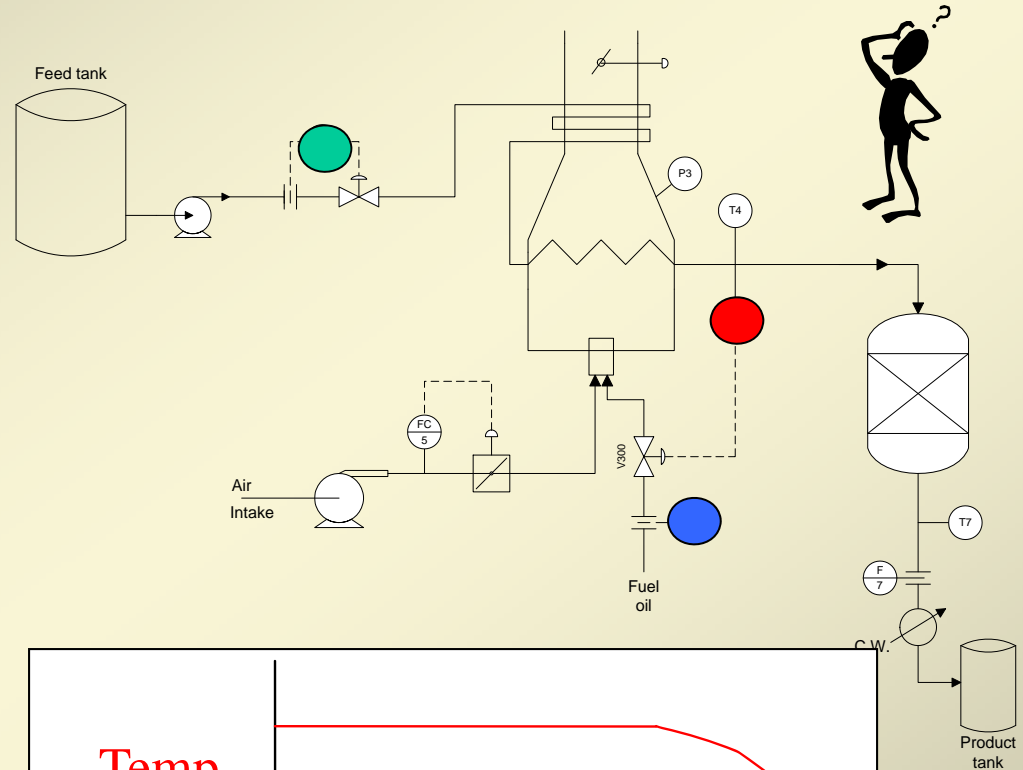
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# MONITORING & DIAGNOSIS

**Systematic Problem Solving Method!**

**Process Trouble Shooting**

1. Engage
2. Define
3. Explore
4. Plan
5. Implement
6. Evaluate

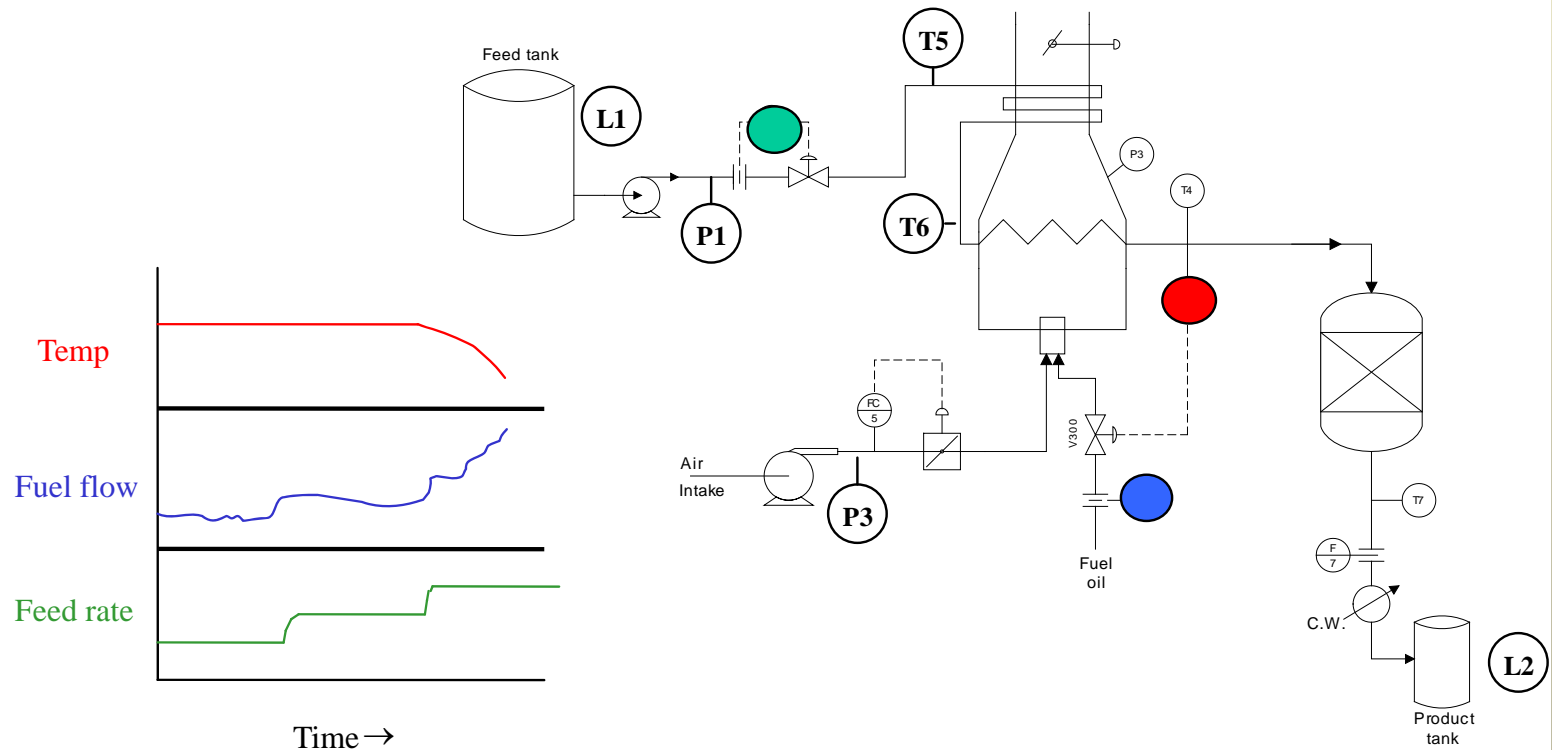


# MONITORING & DIAGNOSIS

## Key Operability issues

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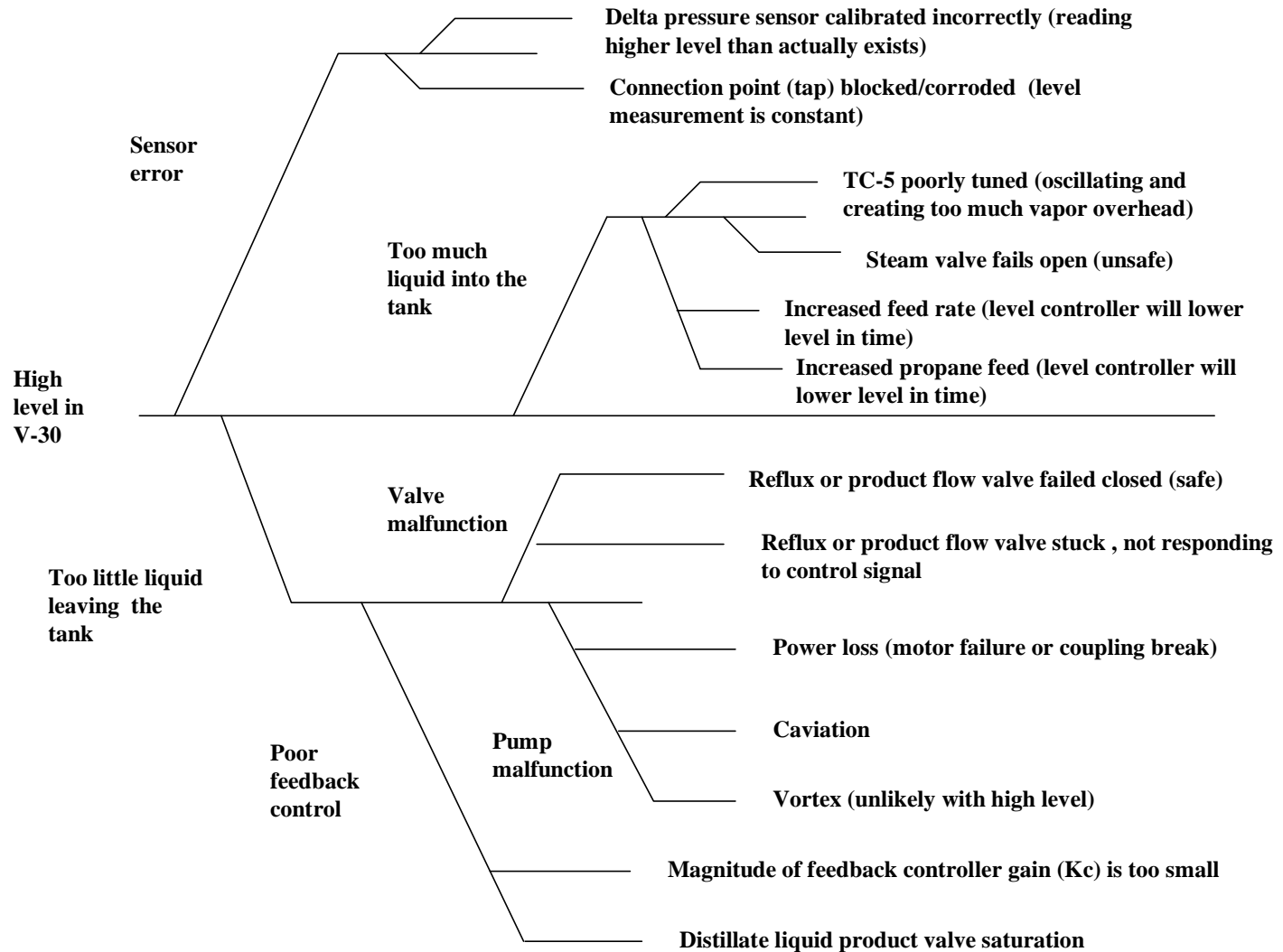
Hypothesis	Initial information	Diagnostic Action
T sensor drift	Neutral	Check with temperature at exit of reactor
Fuel valve is stuck open	Disprove (Temperature would increase)	Place flow controller in manual and make small change to controller output
Feed rate causing T decrease (TC too slow)	Disprove (previous changes were controlled)	-----



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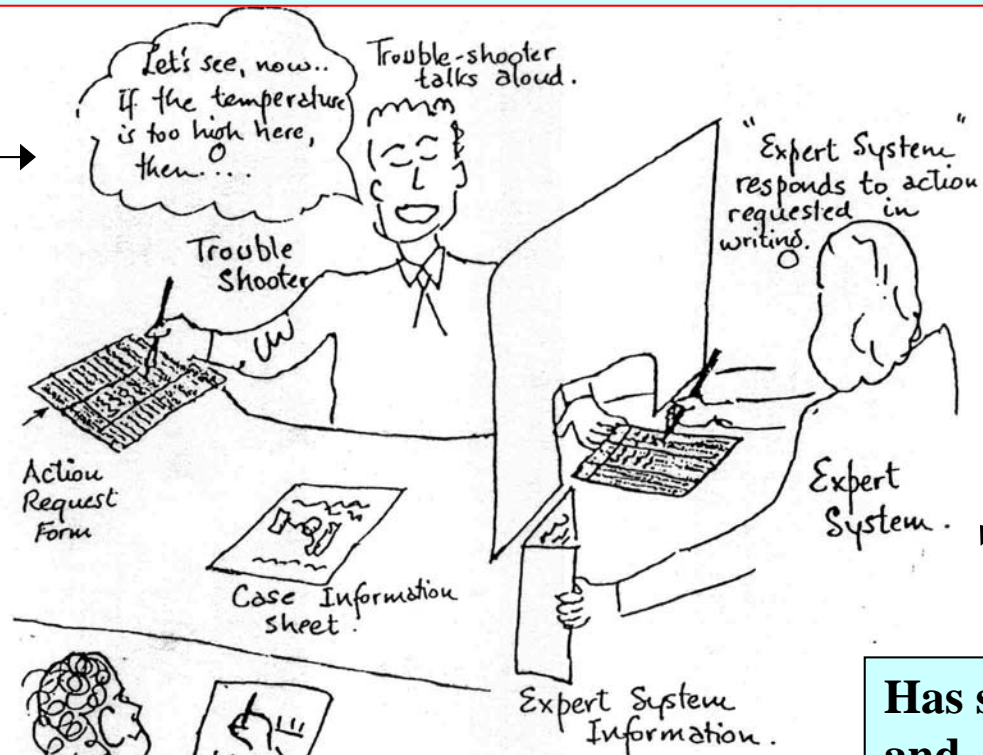
# FISHBONE DIAGRAM FOR MONITORING & DIAGNOSIS





# Student "Triad" Groups for Trouble Shooting Tutorials

Applies the method and verbalizes thinking process



Monitors the TS'ers method and provides feedback after exercise

Has studied the case and provides responses to diagnostic actions (but no hints)

# INSTRUCTOR'S EXPERIENCES

- **Any problem-based teaching style will likely satisfy needs**
- **Heavy load to develop**
- **Operability involves generic topics that are applicable to essentially any process (would have to be modified for product design). See sample projects from previous years.**

- Ammonia reactor and separation loop
- Milk powder evaporators and fluid bed drier
- Municipal water purification plant
- Desalination plant by reverse osmosis
- Ice cream production
- Penicillin production (reactor and separation)
- Refrigeration and cooling tower plant
- Boiler feed water treatment and storage
- Kraft pulp digester
- Wine production

# STUDENTS' EXPERIENCES

## The Good

- Students enjoyed the problem solving tasks (HAZOP and Trouble Shooting)
- Defined diverse projects & found good operability issues



## The Bad

- Difficulty recognizing causes of variability and uncertainty
- Challenge to “work backwards”: effect → cause
- Needed to build experience with qualitative process analysis



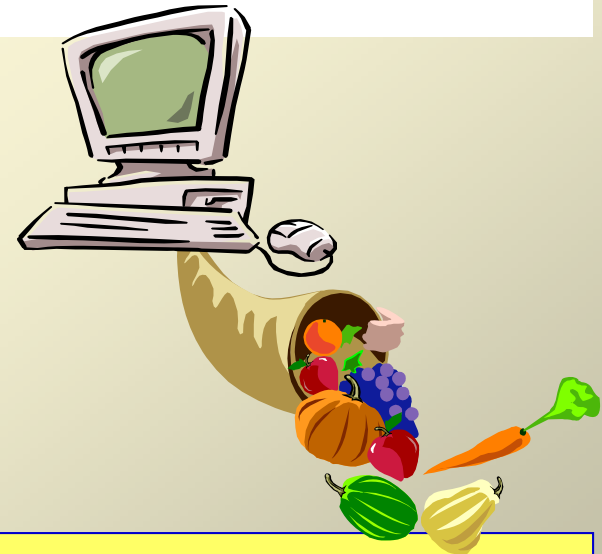
## The Ugly To much work!



# A PROPOSAL FOR Ch.E. INSTRUCTORS

- Integrate **Robust design/process operability** in the capstone design course
- No instructor has experience with all issues
- Limited educational material is available that is accessible to undergraduates

**Proposal to establish a portal for **robust design/ process operability**, with educational materials for public use**

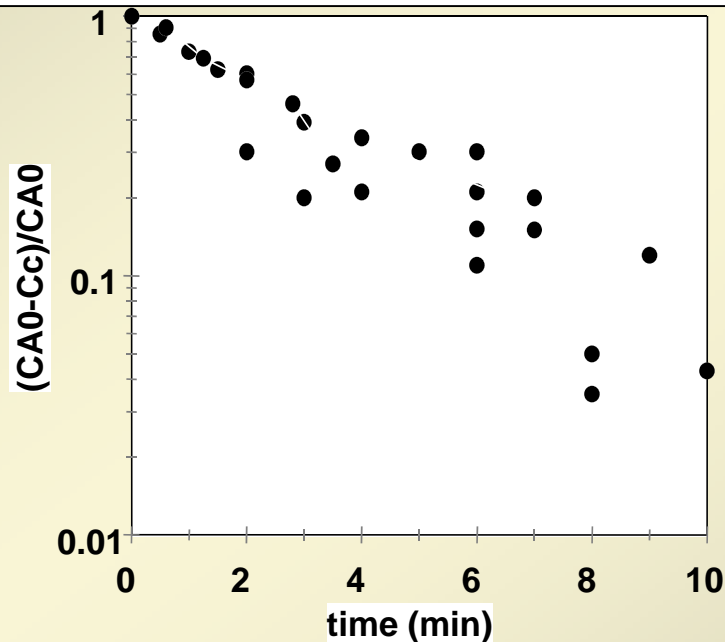


Expanded copy of white paper and power point lessons are available at  
**[www.pc-education.mcmaster.ca/](http://www.pc-education.mcmaster.ca/)**

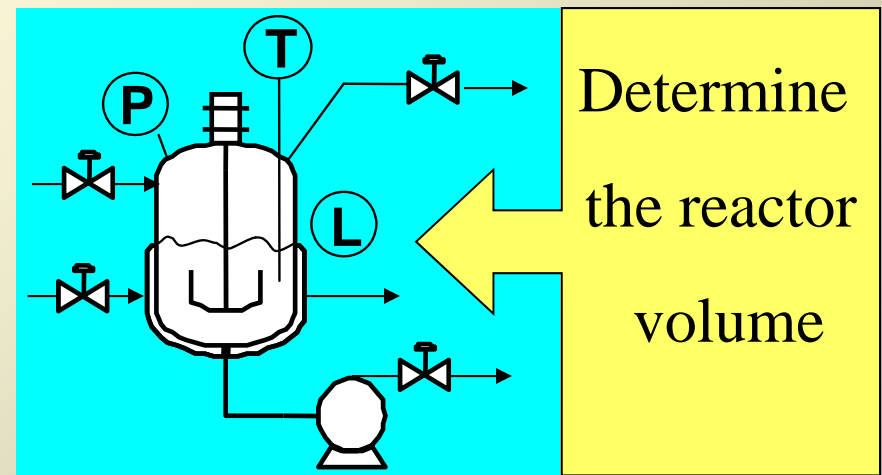
# A RECOMMENDATION FOR PRIOR COURSES

- Typical courses need to introduce causes of variability and uncertainty.
- Solutions should ensure operability (at least in s-s)

## Uncertainty in Rxn kinetics



## Variability in production rate: 70-110% of base design

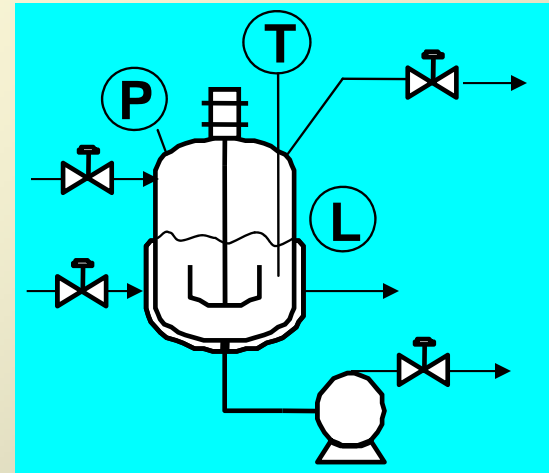


# A RECOMMENDATION FOR PRIOR COURSES

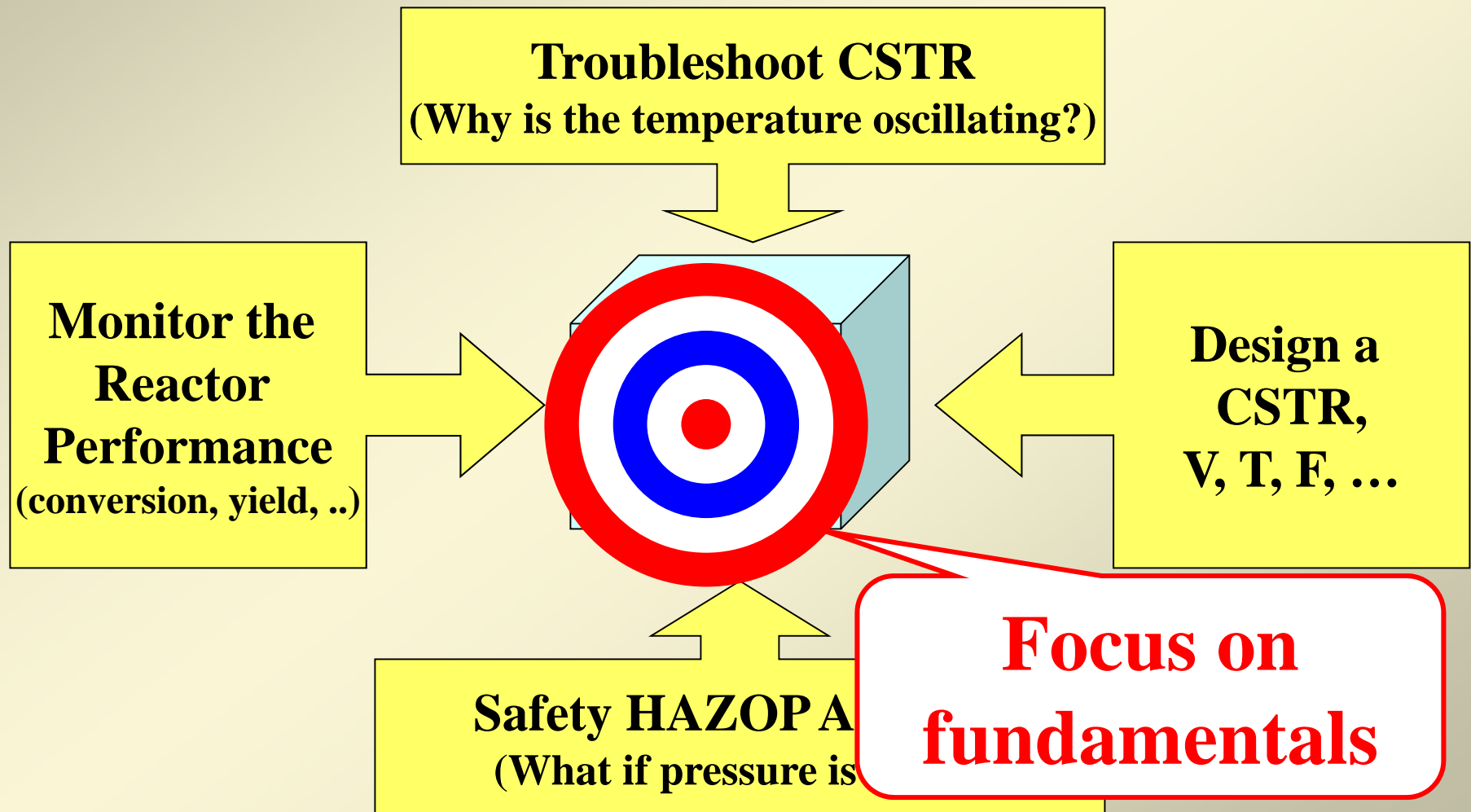
- **Courses need to indicate that processes are changed to achieve desired conditions.**
- **Engineers should be able to analyze the process qualitatively**

We want to increase the feed flow rate by 10% and maintain the conversion unchanged.

What do we do?



**NO NEW PRINCIPLES, but Applications,  
Problem Solving, and Integration are  
Unique**



**Key Operability  
issues**

1. Operating window
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# OPERABILITY IN UNDERGRADUATE EDUCATION



**We would appreciate *comments, criticism, suggestions* at any time, now or by email.**



Key Operability issues

1. Operating window

2. Flexibility/controllability

3. Reliability

4. Safety & equipment protection

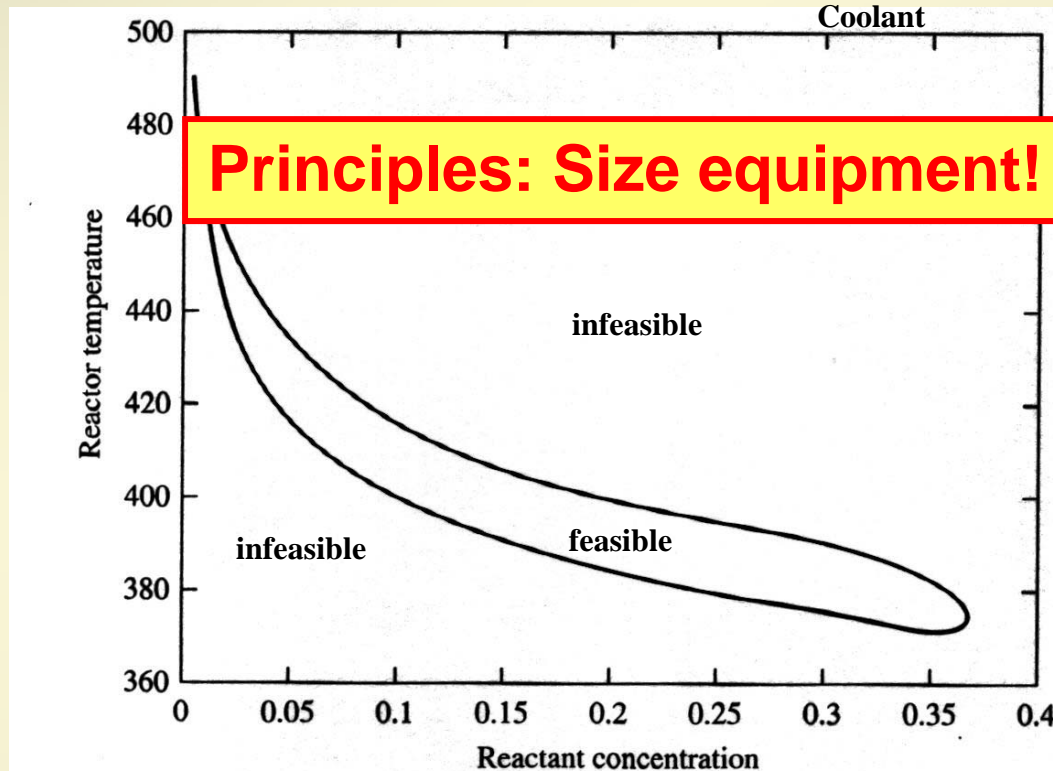
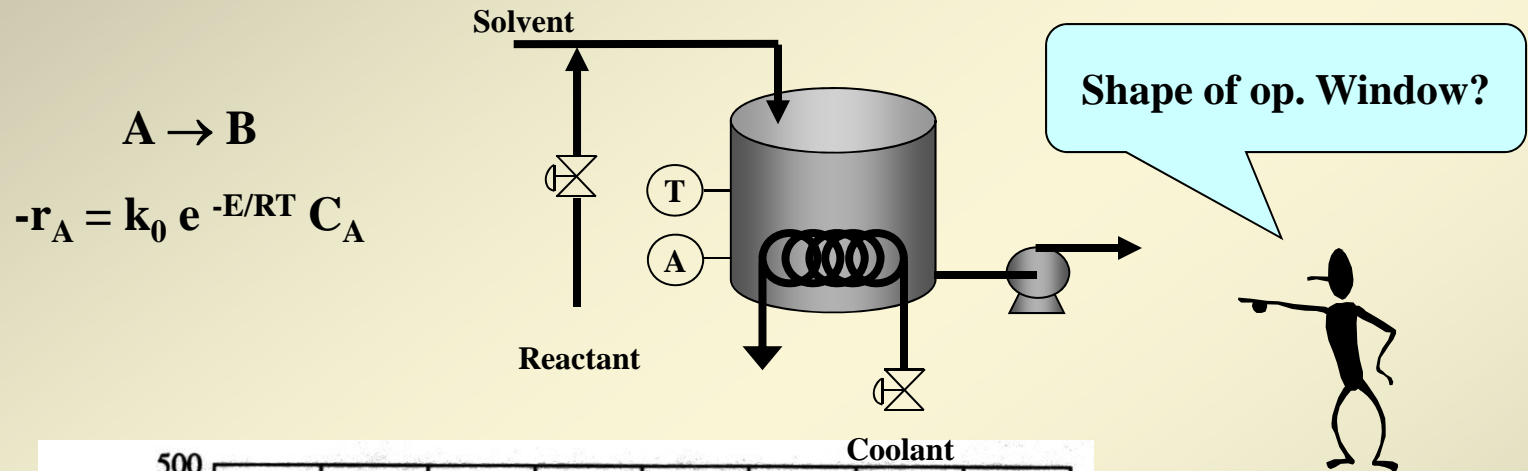
5. Operation during transitions

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# OPERATING WINDOW



- Depends of variability
- Depends on flexibility
- Not rectangular!

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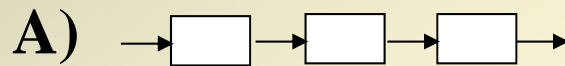
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# RELIABILITY

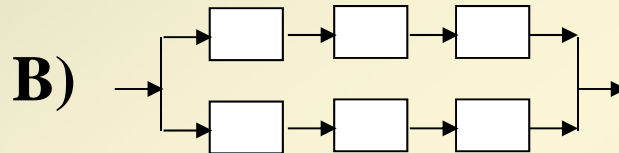
Probability that the process will perform its function properly (one “path” must function)

No redundancy



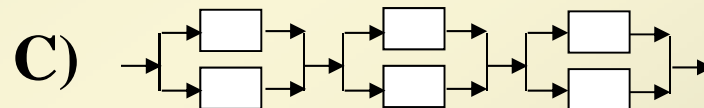
$$R_A = (0.90)^3 = 0.729$$

System-level redundancy



$$R_B = 1 - [1 - (0.90)^3]^2 = 0.927$$

Module-level redundancy



$$R_C = \{1 - [1 - 0.90]^2\}^3 = 0.970$$

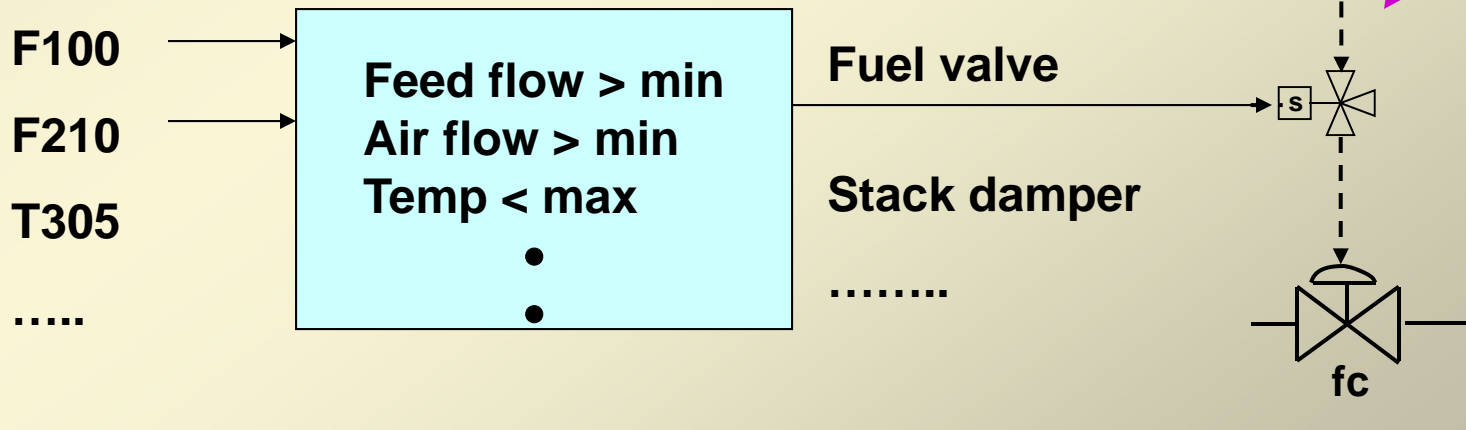
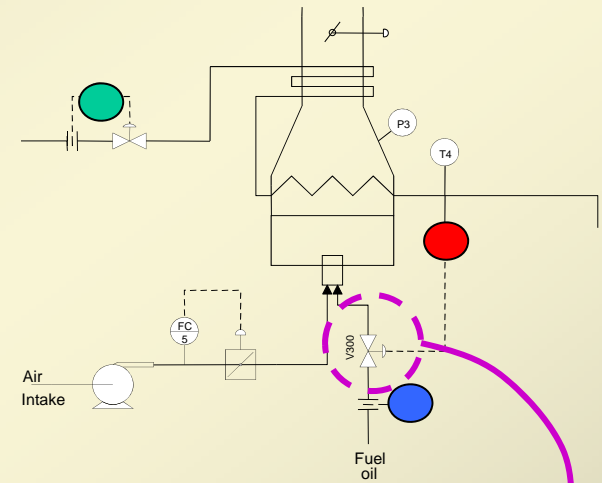
**Increased reliability with increased complexity and cost. We have added redundancy with parallel paths.**

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# SAFETY & EQUIP. PROTECTION

**Learning goals are process principles of SIS: measurements, logic and actions**



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# OPERATION DURING TRANSITIONS

Special equipment and procedures (controls) are required during transition.

## Steady-state processes

- Start-up and shutdown
- Regeneration
- Short runs with frequent switches
- Load following (highly variable demand)

## Unsteady-state processes

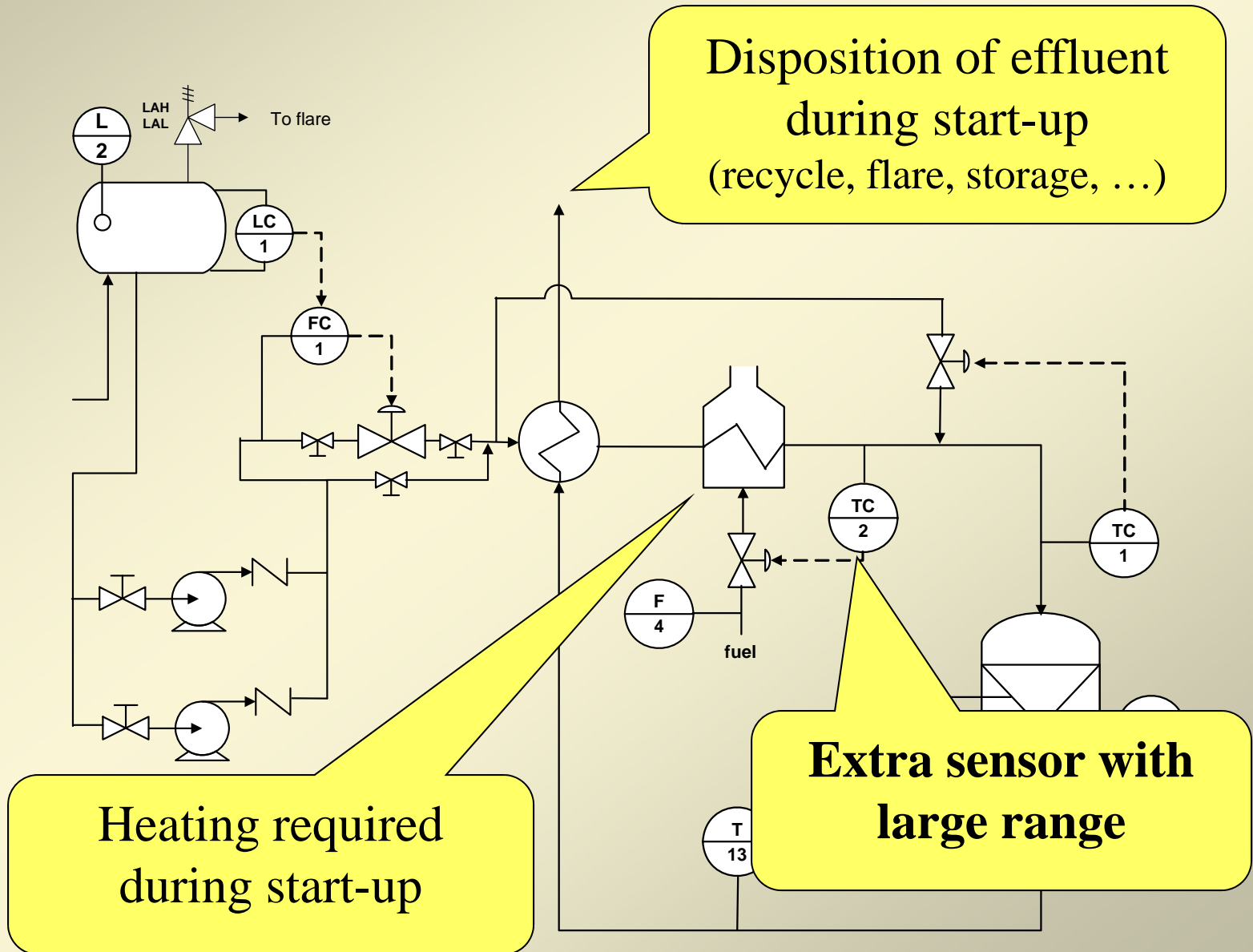
- Batch

**Equipment capacity must satisfy peak demand, not daily or batch average!**

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# OPERATION DURING TRANSITIONS



Disposition of effluent during start-up (recycle, flare, storage, ...)

Heating required during start-up

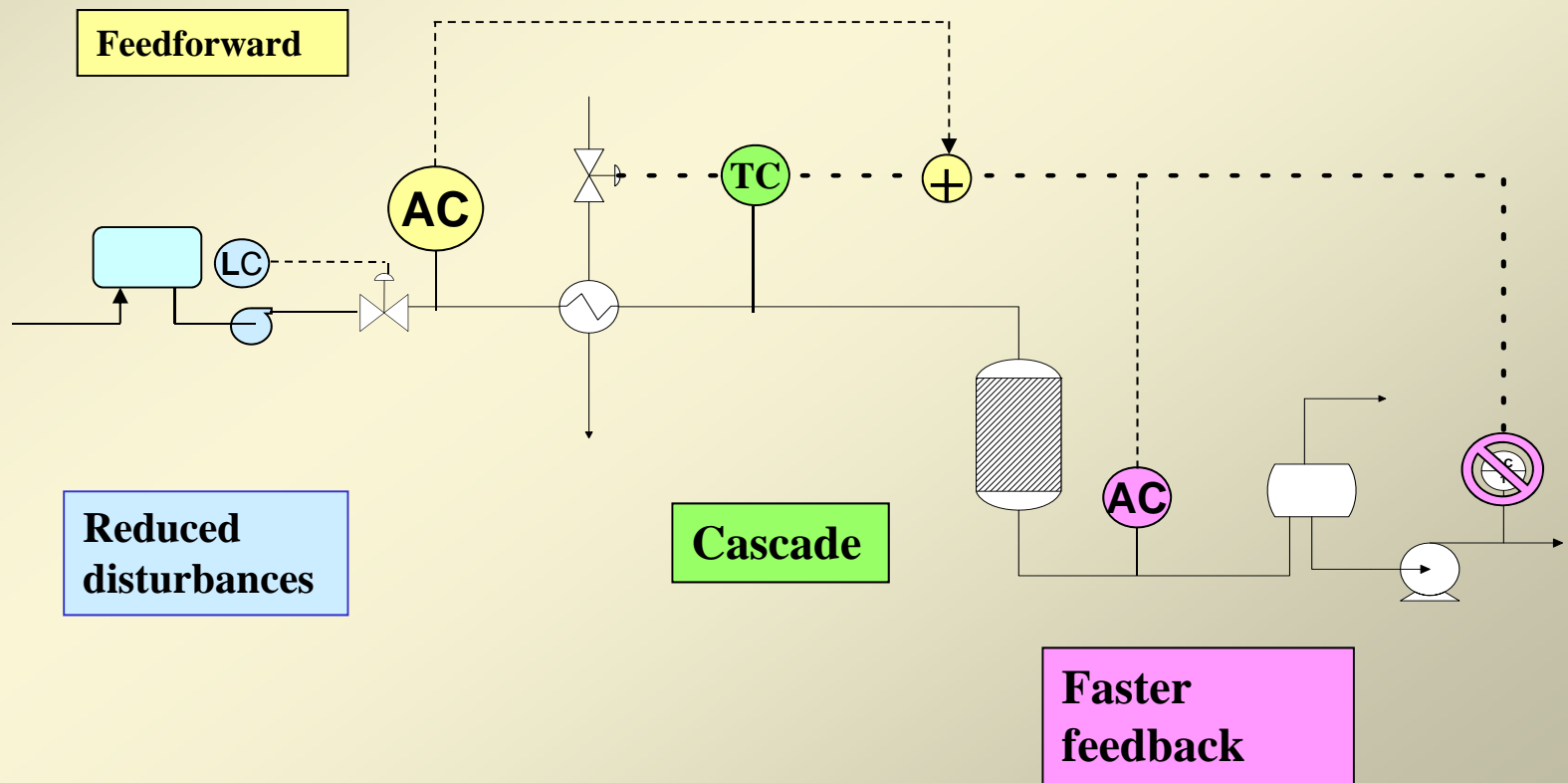
Extra sensor with large range

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# DYNAMIC PERFORMANCE

Rapid compensation for disturbances and timely changes to set points – the **process side** of process control

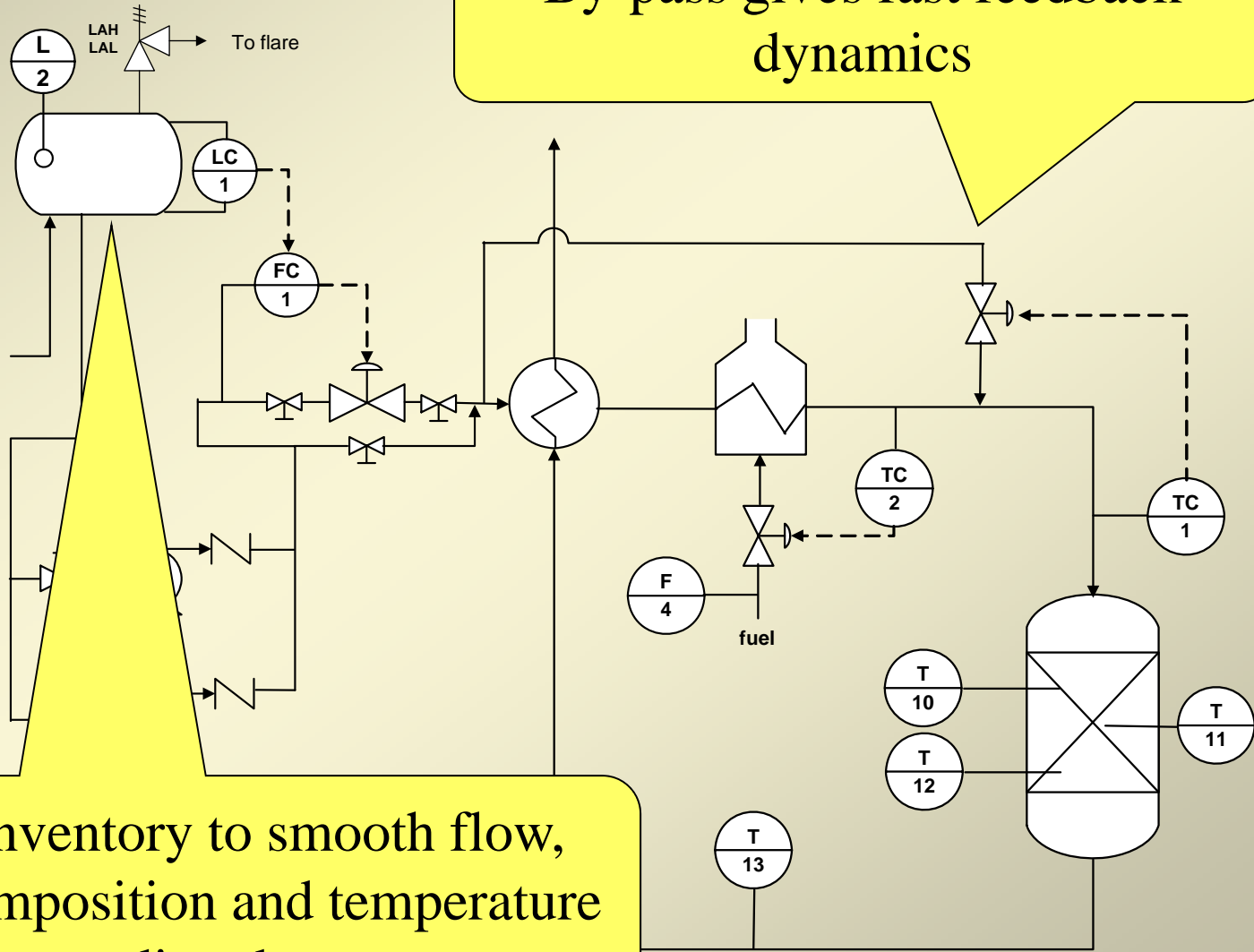


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# DYNAMIC PERFORMANCE

By-pass gives fast feedback dynamics



Inventory to smooth flow, composition and temperature disturbances

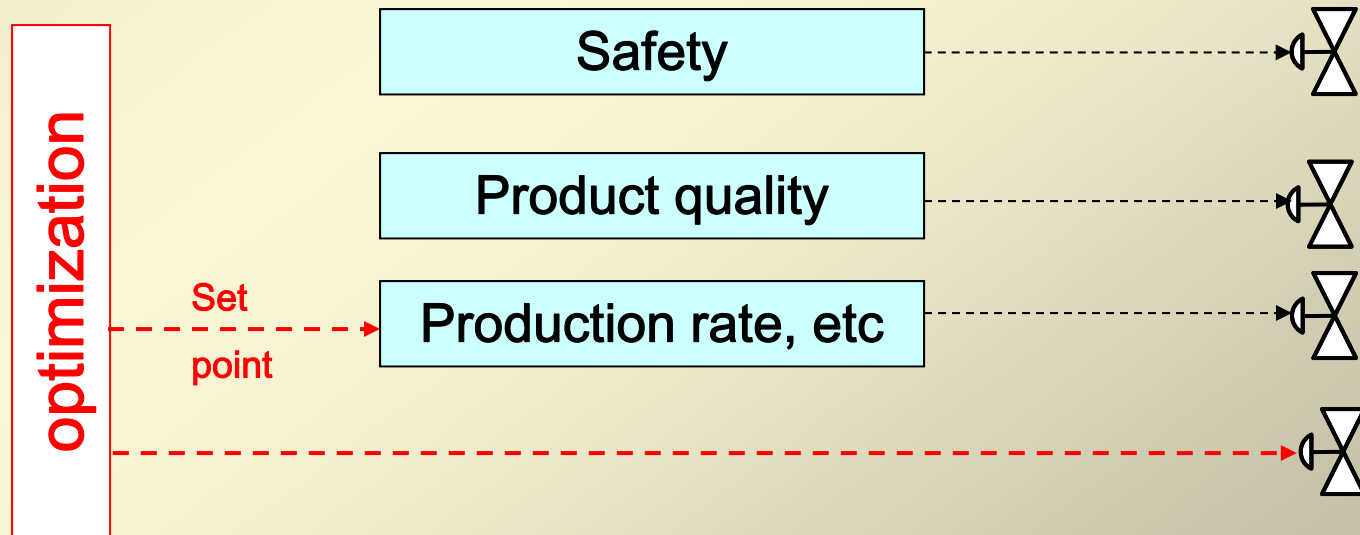
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# EFFICIENCY & PROFIT

With safe, smooth operation making consistently high product quality, is there more to do? **YES!**

**Operability requires extra capacity for extreme situations. We can take advantage during most times to increase profit.**



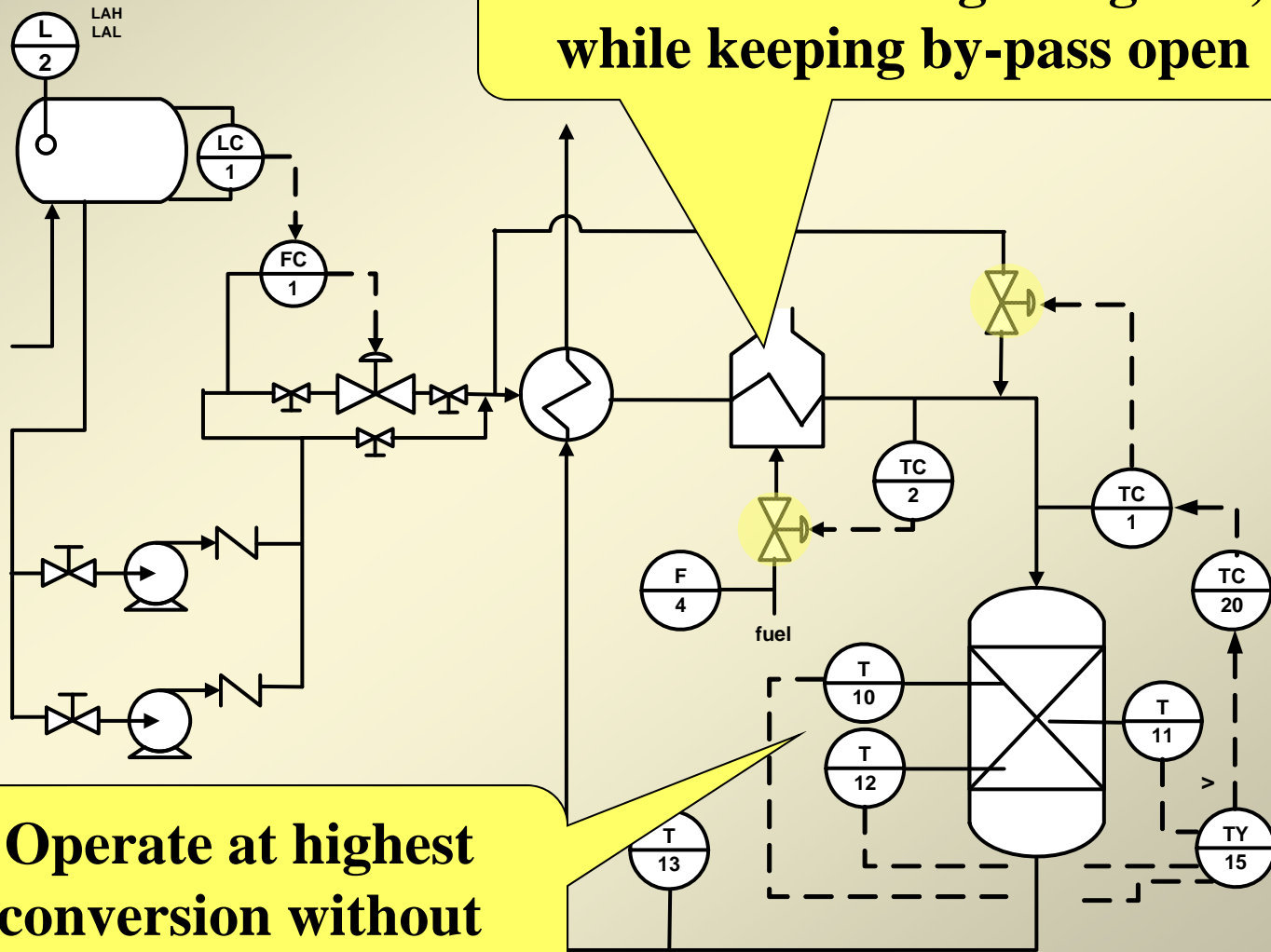


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# EFFICIENCY & PROFIT

**Minimize heating using fuel, while keeping by-pass open**



**Operate at highest conversion without excess temperature**